



Research Article

Measurement of Antioxidant Effects on the Auto-oxidation Kinetics of Methyl Oleate-Methyl Laurate Blend as a Surrogate Biodiesel System

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Abstract

This research investigates the feasibility of methyl oleate-methyl laurate blend as a surrogate biodiesel system which represents jatropha-coconut oil biodiesel, a potentially suitable formulation for tropical climate, to quantify the efficacy of antioxidant additives in terms of their kinetic parameters. This blend was tested by the Rancimat EN14112 standard method. The Rancimat tests results were used to determine the primary oxidation induction period (OIP) and first-order rate constants and activation energies. Addition of BHT and Ecotive™ antioxidants reduces the rate constants (k , h⁻¹) between 15 to 90% in the 50-200 ppm dose range, with Ecotive™ producing significantly lower k values. Higher dose reduces the rate constant, while oleate/laurate ratio produces no significant impact. Antioxidants increase the oxidation activation energy (E_a , kJ/mol) by 180 to almost 400% relative to the non-antioxidant value of 27.0 kJ/mol. Ecotive™ exhibits lower E_a , implying that its higher efficacy stems from a better steric hindrance as apparent from its higher pre-exponential factors. The ability to quantify oxidation kinetic parameters is indicative of the usefulness of methyl oleate-laurate pure FAME blend as a biodiesel surrogate offering better measurement accuracy due to the absence of pre-existing antioxidants in the test samples. Copyright © 2017 BCREC GROUP. All rights reserved

Keywords: Antioxidant; Biodiesel; Oxidation kinetics; Rancimat

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1. Introduction

Global warming is a major global environmental issue that is attributed mainly to the anthropogenic emission of greenhouse gases (GHG), primarily carbon dioxide, methane, nitrous oxide, and fluorinated gases [1]. At the

year 2000 global emission rates, these gases are forecasted by the IPCC (International Panel for Climate Change) to cause global temperature increase between 1.1-6.4 °C and sea level increase between 7-23 inches by the year 2100 [2]. IPCC has also stipulated that GHG emissions must be reduced to 50-85% of the year 2000 rate by 2050 in order to reduce the global temperature rise to an acceptable 2.0-2.4 °C [2]. Of all GHG species, CO₂ by far accounts for the largest portion of the global GHG emis-

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sion. In 2012, global CO₂ emission rate reached 35 billion metric tons per year and is projected to reach 41 billion MTPY by 2020 unless effective emission reduction measures are taken throughout the world [3].

Transportation is the second largest source of anthropogenic GHG emission, contributing to approximately 22% of the global CO₂ emission [4]. Of particular significance in managing emission from the transportation sector is the vast population of automotive diesel engines. Diesel engines offer lower operating costs, higher fuel efficiency, and higher durability than their gasoline counterparts. Naturally, diesel engines are the power plant of choice for commercial and heavy duty on-road and off-road applications. In spite of their advantages, diesel engines suffer from higher particulate (the so-called 'black carbon' emission) and NO_x emissions compared to gasoline engines.

Biodiesel is a generic term for fatty acid methyl esters (FAMEs) derived from animal and plant oils and fats. Compared to petroleum diesel, biodiesel contains more oxygen atoms and lower carbon number. While inevitably resulting in a minor penalty in heating value the higher oxygen content generally results in a cleaner burning fuel compared to petroleum diesel. In one study, 20% substitution of petroleum diesel by biodiesel reduces black carbon emission by 10.1% and residual hydrocarbon emission by 21.1%. The NO_x emission is slightly increased by 2%, while CO₂ emission is virtually unchanged. The CO₂ emission reduc-

tion by biodiesel stems not from its direct emission rates, but from the renewability of the fuel source compared to petroleum [5].

A key problem that is unique to biodiesel is its tendency to undergo auto-oxidation during storage and transportation. The classical theory on FAME auto-oxidation describes the degradation as a two-step process. The primary oxidation stage is described as a chain reaction (see Figure 1). The chain initiation step involves the dehydrogenation of methylene groups, for which allylic and bis-allylic methylene groups are particularly reactive (with relative order of reaction rate of bis-allylic > allylic >> saturated groups). This dehydrogenation forms alkyl radicals, which in the presence of diatomic oxygen react extremely rapidly to form alkyl peroxide radicals in the chain propagation step. The peroxide radicals subsequently dehydrogenate fatty ester molecules to form more alkyl radicals and hydroperoxides / organic acids at a slower rate. Reactions amongst the free radicals to yield stable products constitute the termination step [6].

The hydroperoxide (ROOH) concentration remains low during the initial stages of primary oxidation. After a certain period has passed, the concentration of peroxy radicals has increased to a sufficiently high level such that the ROOH concentration increases rapidly. This period is termed the oxidation induction period (OIP), and is a measure of the resistance of biodiesel to auto-oxidation.

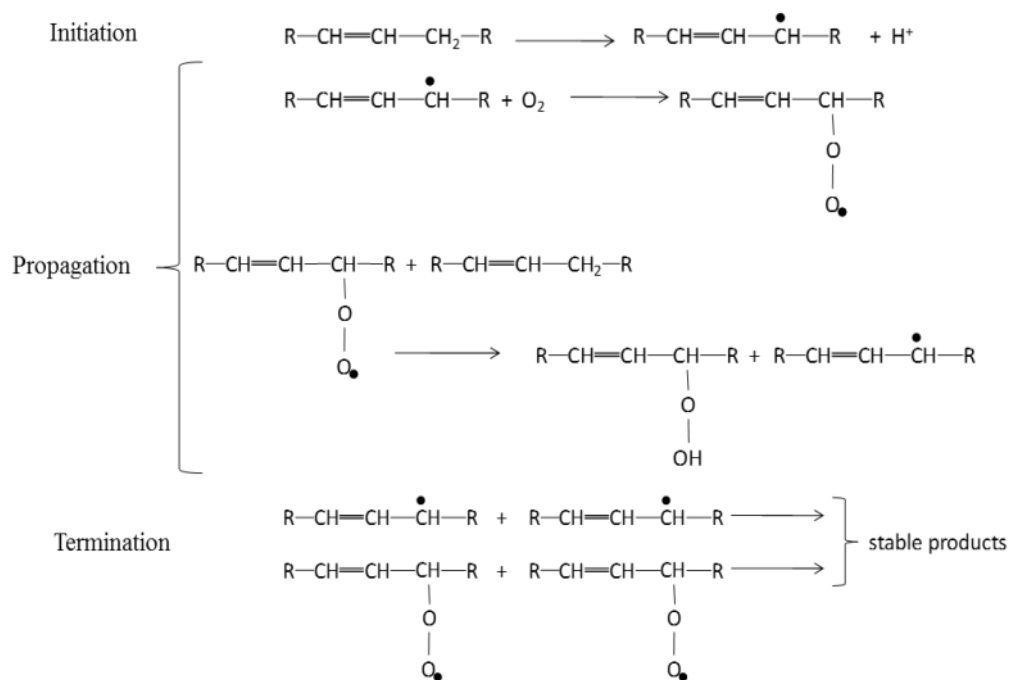


Figure 1. Chain reaction mechanism of the FAME primary oxidation stage

Much more complex hydroperoxide decomposition reactions occur in the secondary oxidation stage, which include dehydration, cyclization, radical substitution, cracking, dimerization, and more. These reactions result in a wide spectrum of products, including monomeric (keto, epoxy, di- and trihydroxy compounds, dihydroperoxides, etc.), oligomeric species which include dimers and trimers linked via peroxy or ether groups, and short-chain species [7]. Formation of oligomeric and short-chain species increase the viscosity of the biodiesel, resulting in poor cold flow behavior and increased filter and nozzle plugging tendency [8]. The secondary oxidation stage is also associated with the formation of shorter-chain fatty acids, which increases biodiesel acidity, and hence its corrosiveness [9].

Various extraneous factors to which the biodiesel is exposed during storage and transportation may accelerate its auto-oxidation. These include temperature, moisture, and ambient air [10]. Presence of certain metals (e.g. copper) has also been argued as accelerant for the auto-oxidation, although with some degree of uncertainty [9]. Conversely, the oxidation stability of biodiesel may be improved by the addition of antioxidants. A pioneering work in the application of antioxidants for biodiesel was described by du Plessis and co-workers [11]. These authors have identified the oxidation retardation effect of phenolic compounds (tert-butylhydroxyquinone / TBHQ) on sunflower oil methyl and ethyl esters. By using the pressurized differential scanning calorimetry (P-DSC) technique in non-isothermal mode, Dunn [12] reported an increase in oxidation onset temperature of soybean oil methyl ester by adding synthetic and natural antioxidants. Synthetic antioxidants used by this author were tert-butylhydroxyquinone (TBHQ), 3-tert-butyl-4-hydroxyanisole (BHA), 2,6-di-tert-butyl-4-methyl phenol or butyl hydroxy toluene (BHT), and n-propyl gallate (PrG). For the natural antioxidant, *α*-tocopherol was used.

Mittelbach and Schober [13] employed the Rancimat method to compare the effectiveness of synthetic antioxidants (TBHQ, pyrogallol, n-propyl gallate, BHA, and BHT) and tocopherols in improving the oxidation stability of several types of biodiesel. Synthetic antioxidants were found to be more effective than natural antioxidants. The generally higher effectiveness of synthetic antioxidants was also observed by Liang and co-workers [14], who studied the effect of antioxidants on crude and distilled palm oil methyl ester. Synthetic antioxidants required only 1/17 of the dose of natural antioxidants to

pass the EN 14214 minimum OIP standard of 6 hours at 110 °C.

The presence of naturally pre-existing antioxidants (such as tocopherols and carotene) in vegetable oils used to synthesize biodiesel results in a wide variation of measured OIP values, even for samples with similar fatty acid compositions [15]. As the observation reported by Liang and co-workers [14] clearly exemplifies, naturally occurring antioxidants in non-distilled palm oil biodiesel produce an OIP of more than 25 hours, compared to only 2.5 hours OIP produced when the palm biodiesel is distilled, effectively removing the natural antioxidants. Thus, the measurement of antioxidant efficacy is prone to interferences from pre-existing, naturally existing antioxidants in the biodiesel itself.

Biodiesel surrogates are blends of FAMEs of known purities and compositions which are formulated to mimic certain physico-chemical characteristics of true biodiesel. While surrogates have been quite extensively used to study biodiesel combustion characteristics (see, for example the works by Herbinet and co-workers [16], and Tao and Lin [17]), their application in the study of auto-oxidation is at best scarce. Being free of pre-existing antioxidants, surrogates may arguably serve as a better matrix compared to true biodiesel in auto-oxidation tests aimed at measuring the intrinsic performance of antioxidants.

This paper discusses the measurement of oxidation kinetics of methyl oleate-methyl laurate blend system as a surrogate jatropha-coconut biodiesel system in the presence of antioxidant additives, with a specific target of quantifying the effect of antioxidants in terms of kinetic parameters of the primary auto-oxidation phase. Selection of jatropha and coconut as the blend components is based on the nature of jatropha as non-edible oil, thus avoiding competitive consumption from the food sector, and on the high auto-oxidation resistance of coconut biodiesel which is attributed to its lack of unsaturated carbon-carbon bonds. Comparison shall be made with kinetic measurement results obtained without antioxidants to highlight the magnitude of efficacy of the antioxidants, and to gain a more comprehensive insight on the role of antioxidants from the reaction kinetics point of view. To the best knowledge of the authors, such use of biodiesel surrogate to measure the OIP performance of antioxidants has never been published to date.

The efficacy of antioxidants in this work is quantified by its first-order kinetic parameters, i.e. rate constant and activation energy. Com-

putation of these parameters directly utilizes the raw conductivity vs. time data measured by Rancimat. This approach is unique, since most published papers on biodiesel auto-oxidation kinetics transforms the OIP values to derive the integrated form of reaction rate expression, which is subsequently used to determine the kinetic parameters [18,19].

2. Materials and Methods

High purity reagent-grade methyl oleate and methyl laurate esters are used (Wako, >99.0%). Since the primary objective of this research is to evaluate the feasibility of using blends of pure FAME as a model biodiesel system in quantifying the kinetic parameters of the auto-oxidation process in the presence of antioxidants, and not to compare the performance of various antioxidants, only two antioxidants are selected for this study. These are butyl hydroxy toluene or BHT (Merck, ≥ 99.0%) and Ecotive™, a proprietary antioxidant.

The major instrument used for this study is the Rancimat Model 743 oxidative stability tester. In the EN14112 standard method, 3-5 grams of the methyl ester sample is contacted with dry air in a heated flask by bubbling. The air bubbles escaping from the sample also strips the volatile short-chain carboxylic acids formed by the primary oxidation stage, which is absorbed by deionized water in a separate absorber flask. The conductivity of the water in the absorber flask increases with an increasing acid concentration in the air transferred from the sample flask. A sharp increase in the conductivity indicates that the oxidation reaction has progressed to the secondary stage, and the time period required to reach this sharp increase in conductivity is recorded as the OIP.

The experimental work in this study involves two parts, namely a preliminary experiment aimed at identifying the appropriate range of antioxidant dose, and a main experiment which measures the kinetic parameters of the oxidation process in the absence and presence of antioxidants. Experimental factors of interest are oleate/laurate volumetric blending

ratio, Rancimat oxidation temperature, and antioxidant type and dose. Table 1 compiles all experimental factors and their respective values selected in this study.

Determination of kinetic parameters is based on first-order reaction kinetic treatment of the water absorber conductivity versus time raw data generated by Rancimat. This simple approach is taken on the assumption that the water absorber conductivity is linearly correlated to the concentration of ROOH produced by the oxidation. Similar approach has also been employed in published literature to determine oxidation rate constants and activation energy of true biodiesels [18,20]. The water absorber conductivity vs. time data are also used to determine the OIP values, although these are not directly related to the kinetic parameters sought after in this work.

3. Results and Discussion

3.1. Determination of antioxidant dose range

In this preliminary part of the evaluation of antioxidant effects on the oxidation of methyl oleate-laurate blends, the effect of BHT and Ecotive™ antioxidant concentration is measured by adding selective doses (25, 50, 100, and 200 ppm) of the antioxidants to pure methyl oleate. The methyl oleate samples which have been added with antioxidants are then tested by the Rancimat instrument at 110 °C. Neat methyl oleate is selected for the preliminary experiment since it is naturally the most easily oxidized among the oleate-laurate blending ratio values selected in this research.

The OIP values are determined from the raw conductivity vs. time data in accordance to the ‘manual method’ described in EN 14214. Figure 2 presents an example of how such determination is undertaken. This particular example refers to the oxidation of methyl oleate with the addition of 100 ppm BHT. Tangent lines are drawn along the linear regions with low slope (representing the initial stages of the primary oxidation phase, where the produced acid concentration is still low) and that with

Table 1. Experimental factors and levels

Factors	Values
Oleate/laurate volumetric ratio	40/60, 60/40, 80/20, 100/0
Oxidation temperature, °C	90, 100, 100
Antioxidant type	BHT, Ecotive™
Antioxidant dose, ppm	0, 50, 200

high slope (the earlier stages of the secondary oxidation phase). These tangent lines are extended, and the point at which they intersect is taken as the OIP.

Table 2 summarizes the OIP values obtained by the Rancimat method at the selected antioxidant dose levels. The OIP values vary linearly with the antioxidant dose level. For pure methyl oleate, OIP values obtained by adding Ecotive™ are 4-5 times longer than those obtained by using BHT. At a dose of up to 200 ppm, BHT fails to produce OIP which passes the EN minimum value of 6.0 hours, while Ecotive™ is able to delay the onset of methyl oleate oxidation to more than 6.0 hours at a dose of 50 ppm. Based on these results, and to obtain a more direct comparison between BHT and Ecotive™, the low and high doses for the subsequent main experiment are set at 50 and 200 ppm respectively for both antioxidants.

It should be reiterated here that the objective of this research is not to find the optimum antioxidant type and dose, but rather to evaluate the impact of antioxidants on the kinetic

parameters of the primary oxidation stage of biodiesel. The choice of low and high antioxidant doses of 50 and 200 ppm, respectively, is aimed at producing sufficient difference in the IP response values, while avoiding an excessively long IP values which would tend to decrease the precision of oxidative stability measurements.

3.2. Primary oxidation kinetic parameters measurement

Measurement of the primary auto-oxidation kinetic parameters is undertaken through a series of Rancimat oxidation tests with experimental factors set according to Table 1. Fundamentally, the intrinsic oxidative stability of pure methyl esters is determined by the number of unsaturated carbon-carbon bonds in the molecules. This premise leads to the description of oxidation propensity in terms of structural parameters that expresses the degree of bond saturation (or unsaturation) of the methyl esters [21]. One such parameter is the degree of unsaturation (DU) proposed by Ramos [22], which is calculated from the fatty acid (FA) composition of the biodiesel sample by Equation (1):

$$DU = X_{FA,u} + 2X_{FA,pu} \quad (1)$$

where DU = degree of unsaturation (%); $X_{FA,u}$ = %-mass of mono-unsaturated fatty acids; and $X_{FA,pu}$ = %-mass of polyunsaturated fatty acids.

Table 3 lists the calculated DU values of the methyl oleate-laurate blends used in this work and several neat biodiesel obtained from the literature. Of the considerable wealth of data on jatropha, palm and coconut methyl esters available in the public literature, only those accompanied by their fatty acid composition data can be used for DU calculation by Equation (1) [23-25].

Methyl oleate-laurate blend Rancimat OIP values are plotted against DU in Figure 3. Error bars corresponding to 95% confidence interval of the average OIP values of each sample are included, computed from three replicate runs. Also included in the figure are several literature OIP values of neat biodiesels listed in Table 3. Excellent repeatability of the methyl oleate-laurate blend OIP measurements was obtained with the Rancimat test, as indicated by the measurement confidence intervals that are much narrower compared to the overall OIP value range. The OIP values of the methyl oleate-laurate blends exhibits a strong linear correlation with the DU parameter.

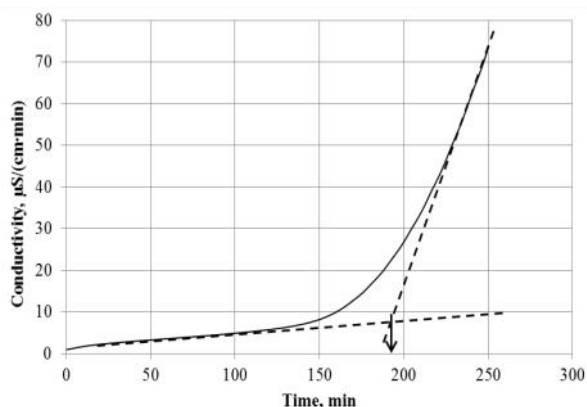


Figure 2. Water absorber conductivity raw data of the oxidation of methyl oleate at 110 °C with the addition of 100 ppm BHT, indicating the determination of OIP using the tangent intersection method

Table 2. Methyl oleate rancimat OIP at varying antioxidant doses at 110 °C

Antioxidant dose, ppm	Rancimat OIP, hrs	
	BHT	Ecotive™
0	0.68	0.68
25	1.40	5.70
50	2.08	9.50
100	3.22	15.7
200	5.67	29.0

Figure 3 very clearly indicate the discrepancy of measured OIP of the surrogate biodiesel and the true, neat biodiesels with equivalent DU values. All of the neat biodiesels exhibit much longer OIP values than pure FAME blends. This observation indicates that the oxidative stability of true biodiesels is determined to a much larger extent by pre-existing antioxidants rather than their fatty acid composition. The palm biodiesel OIP data from Frohlich and Schober [24] are of particular interest, since these authors compare the methyl esters produced from crude palm oil and from palm oil which had been treated by activated carbon to remove the naturally-occurring tocopherols. Despite this adsorption treatment, the OIP of the palm biodiesel was

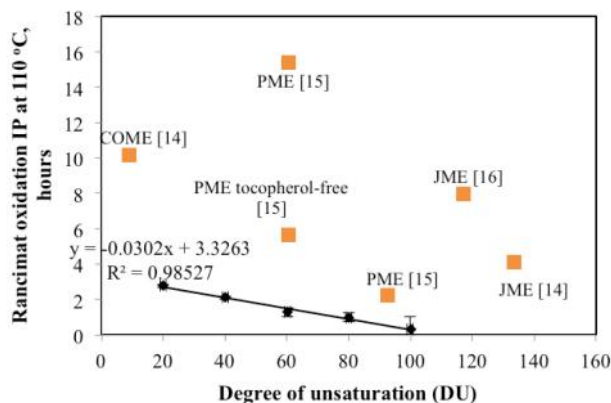


Figure 3. Rancimat OIP measured at 110 °C of methyl oleate - laurat blends and several neat biodiesels as a function of the degree of unsaturation

still significantly higher than the corresponding methyl oleate-laurate blend (at a DU of approximately 60%), suggesting an incomplete tocopherol removal or the presence of other antioxidant species not removed by the activated carbon adsorbent. It is therefore clear that the quantification of antioxidant efficacy using true biodiesel is extremely prone to pre-existing antioxidants.

By assuming that the primary oxidation stage follows first-order kinetics, rate constants may be determined by computing the slope of $\ln(\text{conductivity})$ vs. time plots. Figure 4 presents first-order plots of the oxidation of methyl oleate-laurate blends at 90 °C as an example of the kinetic data treatment results. After an initial warm-up period which lasts for approximately 15 minutes, the curves in Figure 2 exhibit a linear behavior in accordance with first-order kinetics. Indeed, such first-order kinetic behavior is also observed by Nakatani and co-workers [26]. The rate constants of the primary oxidation stage were determined simply by taking the slope of the $\ln(\text{Conductivity})$ vs. time curves in the linear regions, and are compiled in Table 4.

Treatment of Rancimat data for methyl oleate-laurate oxidation with antioxidants is analogous to that of the experiments without using antioxidants. Figure 5 presents the first-order plots for the oxidation at 100 °C with the addition of 50 ppm BHT as an example. Comparison of the curves in Figures 4 and 5 confirms that the oxidation of methyl oleate-laurate blends in the presence of antioxidants

Table 3. Calculated degree of unsaturation (DU) of several types of FAME

Methyl ester / biodiesel samples	Degree of unsaturation (DU)	Reference
Methyl oleate-methyl laurate blends:		
20/80	20.08	This work
40/60	40.13	This work
60/40	60.13	This work
80/20	80.08	This work
100/0	100.00	This work
Neat biodiesels:		
Coconut biodiesel	8.81	[23]
Jatropha biodiesel	133.35	[23]
Palm biodiesel	92.68	[23]
Palm biodiesel	60.60	[24]
Palm biodiesel, natural tocopherols removed	60.60	[24]
Jatropha biodiesel	117.11	[25]

also follows first-order kinetics. In a similar manner to the experiments without antioxidants, rate constants of methyl oleate-laurate oxidation in presence of BHT and Ecotive™ antioxidants are determined from the slope of ln(Conductivity) vs. time curves. These are also compiled in Table 4.

As the numbers in Table 4, and the curves in Figures 4 and 5 suggest, the rate constant values are not substantially influenced by the oleate/laurate blending ratios while obviously influenced by the initial concentration (or dose) of the antioxidants. This observation supports the underlying concept of oxidation kinetic modeling in the literature, in which the rate of oxidation in presence of antioxidants is associated with the consumption of the antioxidant itself [19]. Experimental runs undertaken at the four blend ratios are thus regarded as repli-

cates in computing 95% confidence intervals of the rate constant at each combination of temperature and antioxidant dose. The averaged rate constants are summarized in Table 5.

The activation energies of the primary auto-oxidation with and without antioxidants are then determined using the classical Arrhenius equation:

$$k = Ae^{-E_a/RT} \quad (2)$$

where k = first-order rate constant (h^{-1}); A = pre-exponential factor (h^{-1}); E_a = activation energy (kJ/mol); R = ideal gas constant = $8.314 \text{ kJ/mol} \cdot \text{K}$; and T = reaction temperature (K).

The activation energies are determined from the slope of $\ln(k)$ vs. $1/T$ plots. The Arrhenius plots encompassing all experimental runs are compiled in Figure 6, which also in-

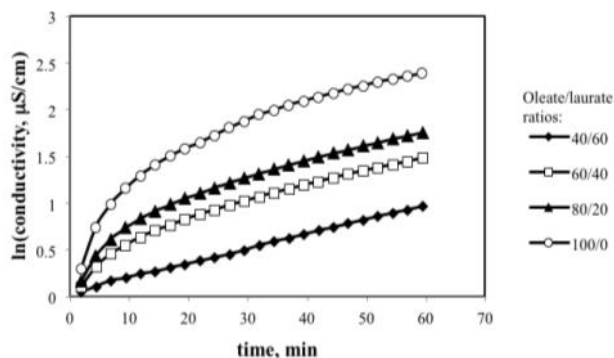


Figure 4. First-order kinetic plot of methyl oleate-laurate blend Rancimat oxidation at 90 °C

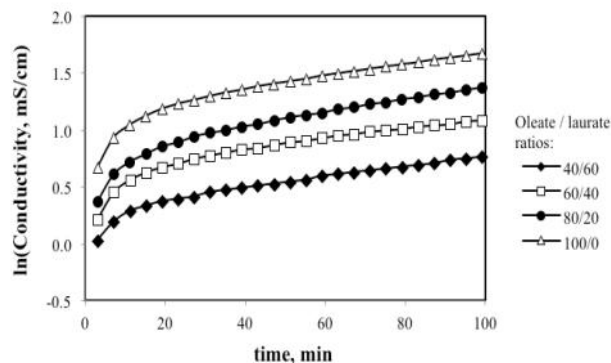


Figure 5. First-order kinetic plot of methyl oleate-laurate blend Rancimat oxidation in the presence of 50 ppm BHT at 100 °C

Table 4. Methyl laurate – oleate blend oxidation rate constants with and without the addition of antioxidants obtained by the Rancimat method

T, °C	oleate/laurate blending ratio	k , hour ⁻¹				
		No antioxidant	BHT 50 ppm	BHT 200 ppm	Ecotive™ 50 ppm	Ecotive™ 200 ppm
90	40/60	0.861	0.114	0.0404	0.103	0.03096
	60/40	0.762	0.12	0.0469	0.099	0.03234
	80/20	0.924	0.126	0.0402	0.108	0.02934
	100/0	0.897	0.096	0.0392	0.079	0.03222
100	40/60	0.900	0.276	0.150	0.204	0.066
	60/40	1.020	0.276	0.180	0.184	0.078
	80/20	1.083	0.354	0.162	0.210	0.078
	100/0	1.188	0.324	0.186	0.216	0.076
110	40/60	1.287	1.212	0.354	0.312	0.136
	60/40	1.425	1.124	0.372	0.376	0.109
	80/20	1.377	1.17	0.324	0.366	0.114
	100/0	1.398	1.152	0.390	0.390	0.128

cludes the average rate constant 95% confidence intervals. The activation energies are summarized in Table 5, also as 95% confidence intervals. Confidence intervals of the rate constants and activations energies are reasonably narrow, suggesting a good overall measurement precision.

Table 4 and Figure 6 confirm the significant change in kinetic parameters caused by the addition of antioxidants, specifically the increase in activation energy. This is to be expected in the context of antioxidants as reaction inhibitors, which works oppositely to a catalyst in

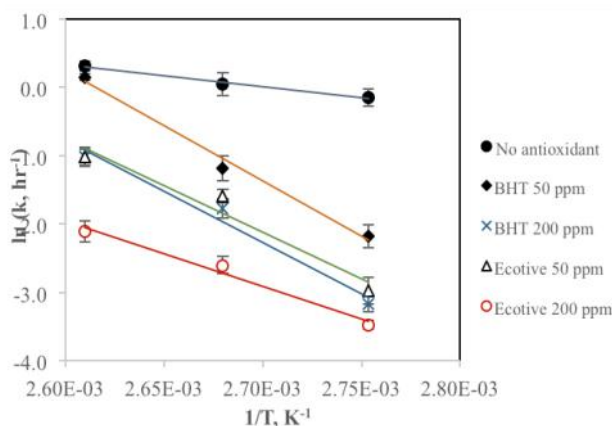


Figure 6. Arrhenius plots of methyl oleate – laurate blend oxidation based on first-order reaction kinetics

that it provides a new reaction pathway with a higher activation energy compared to the non-inhibited pathway. The first-order kinetic analysis of the Rancimat data is also able to quantitatively distinguish the performance of BHT and Ecotive™. While the latter antioxidant provides lower rate constants and longer OIP, the obtained activation energy is actually lower than that obtained by adding BHT. In this case the pre-exponential factor in the Arrhenius equation has a larger impact on the oxidation rate compared to the activation energy, suggesting that Ecotive™ may provide more steric hindrance to the oxidation reaction relative to BHT.

Increase of antioxidant dose from 50 to 200 ppm does not appear to significantly change the activation energy for either BHT or Ecotive™, as the 95% confidence intervals in Table 5 suggest. The activation energy of BHT obtained in this work is significantly higher than values reported in the literature. Borsato and co-workers [20] reported an activation energy of 81.72 kJ/mol for the oxidation of soybean oil B100 biodiesel with the addition of approximately 1000 ppm BHT. Jain and Sharma [27] reported activation energy of jatropha B100 biodiesel containing BHT that increases linearly with antioxidant dose, based on non-isothermal first-order kinetic data treatment. These authors obtain activation energy values

Table 5. Average rate constants and activation energies of methyl oleate-laurate oxidation

Antioxidant	Dose, ppm	T, °C	k , h ⁻¹	E_a , kJ/mol	A , h ⁻¹
None	-	90	0.861 ± 0.113	27.0 ± 3.5	$6.48 \cdot 10^3$
		100	1.048 ± 0.191		
		110	1.372 ± 0.095		
BHT	50	90	0.114 ± 0.021	134.5 ± 5.8	$2.34 \cdot 10^{18}$
		100	0.308 ± 0.061		
		110	1.164 ± 0.059		
	200	90	0.042 ± 0.005	125.0 ± 7.1	$4.42 \cdot 10^{16}$
		100	0.170 ± 0.026		
		110	0.360 ± 0.045		
Ecotive™	50	90	0.097 ± 0.020	76.1 ± 4.4	$8.82 \cdot 10^9$
		100	0.204 ± 0.022		
		110	0.361 ± 0.054		
	200	90	0.031 ± 0.002	78.7 ± 4.7	$6.94 \cdot 10^9$
		100	0.074 ± 0.010		
		110	0.122 ± 0.020		

in the 42.96 to 57.06 kJ/mol range for BHT dose of 100 to 600 ppm. The difference between values reported in the literature, which are measured by using real biodiesel samples, and those reported in Table 5 highlights once again the risk of interference from pre-existing antioxidants (and also pro-oxidants) inherently present in real biodiesel in the rigorous measurement of oxidation kinetic parameters.

4. Conclusions

The direct treatment of Rancimat conductivity vs. time raw data according to first-order kinetics has been demonstrated to be able to quantify the effect of antioxidants on biodiesel primary oxidation in terms of changes in the rate constants and activation energies. The use of jatropha-coconut biodiesel surrogate in the form of blends of pure methyl oleate and methyl laurate enables the determination of intrinsic kinetic parameters of the auto-oxidation process. It has been confirmed that kinetics of the auto-oxidation in presence of BHT and Ecotive™ antioxidants refers to the consumption of antioxidants in the primary oxidation phase. Increasing the antioxidant dose from 50 to 200 ppm reduces the rate constants by 63-39%. Oxidation activation energy of the biodiesel surrogate increases 3.6-4.0 times with BHT, and 1.8-1.9 times with Ecotive™, confirming the role of antioxidants as reaction inhibitors. To validate the applicability of biodiesel surrogate in the quantification of antioxidant efficacy, similar tests with a wider range of antioxidants is recommended for future studies .

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